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Phosphorus poisoning during wet oxidation of methane over Pd@CeO₂/graphite model catalysts



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ABSTRACT

The influence of phosphorus and water on methane catalytic combustion was studied over $Pd@CeO_2$ model catalysts supported on graphite, designed to be suitable for X-ray Photoelectron Spectroscopy/Synchrotron Radiation Photoelectron Spectroscopy (XPS/SRPES) analysis. In the absence of P, the catalyst was active for the methane oxidation reaction, although introduction of 15% H $_2O$ to the reaction mixture did cause reversible deactivation. In the presence of P, both thermal and chemical aging treatments resulted in partial loss of activity due to morphological transformation of the catalyst, as revealed by Scanning Electron Microscopy (SEM) and Atomic Force Microscopy (AFM) analysis. At 600 °C the combined presence of PO_4 and water vapor caused a rapid, irreversible deactivation of the catalyst. XPS/SRPES analysis, combined with *operando* X-ray Absorption Near Edge Structure (XANES) and AFM measurements, indicated that water induces severe aggregation of CeO_2 nanoparticles, exposure of $CePO_4$ on the outer layer of the aggregates and incorporation of the catalytic-active Pd nanoparticles into the bulk. This demonstrates a temperature-activated process for P-poisoning of oxidation catalysts in which water vapor plays a crucial role.

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1. Introduction

Palladium-based catalysts are the most active materials for oxidation of methane at low temperatures [1,2], and especially high activity can be achieved when the Pd is in the presence of reducible promoters such as ceria (CeO₂) [3–5]. The promoter helps stabilize PdO (the most active phase) against thermal decomposition to less active Pd, improving the catalytic performance by activation and spillover of oxygen from the promoter to the Pd phase [2,4,5]. Indeed, recent work has shown that the activity of ceria-supported Pd catalysts increases with the interfacial contact between the Pd phase and ceria [6]. Therefore, to maximize this contact, some of us recently used self-assembly methods to synthesize

hierarchical, core–shell catalysts, designated here as Pd@CeO₂, that consist of Pd nanoparticles surrounded by a thin porous shell of ceria [7]. These catalysts show remarkable activity for CH₄ combustion under some conditions and offer significant potential to improve the performance of catalysts required to reduce methane emissions. However, despite their high intrinsic activity for methane oxidation, Pd-based catalysts can deactivate under real conditions, especially in the presence of water vapor, sulfur and phosphorus species [8–14].

Phosphorus is a particularly serious poison for CeO_2 -promoted catalysts and is a primary agent for irreversible deactivation of automotive catalytic converters under real operating conditions [15–17]. The presence of phosphorus compounds $(P_2O_5 \text{ or } H_3PO_4)$ in vehicle exhaust is due to decomposition/volatilization of motor oil anti-wear additives, such as zinc dialkyldithiophosphate (ZDDP) [18,19]. These additives are present in most available motor oils in concentration up to 1–2% (although this can vary depending on

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the final application) and their effect on catalytic converters is well documented [15–17]. Based on studies of simplified, model systems (CeO₂ and Ce_xZr_{1-x}O₂) [18–25], it is known that mixed phosphates (Zn, Ca and Mg) form glassy overlayers on the washcoat surface and also react with the catalyst to form CePO₄ and AlPO₄ [25].

CePO₄ formation is irreversible and detrimental to the catalytic activity due to loss of oxygen storage capacity (OSC), which is caused by locking of the Ce³⁺/Ce⁴⁺ pair in the 3+ state [24,25]. Both the direct reaction of CeO₂ with phosphorus compounds in the gas phase and the reaction of CeO₂ with P-containing species on the catalyst (e.g. aluminum phosphate) can lead to the formation of CePO₄ [22]. Based on evidence from total reflection X-ray fluorescence (TXRF), XPS and ³¹P NMR data on P-poisoned CeO₂, phosphate species formed on the surface and sub-surface region dramatically decrease OSC. Cerium phosphate is also very stable and cannot be removed from either pure CeO_2 or $Ce_xZr_{1-x}O_2$ by calcination treatments to 1000 °C [21,26]. A few studies indicated partial removal of phosphate species by washing the spent catalyst with oxalic acid [18] or chlorine containing species [27]. However, CePO₄ persists even after these treatments [18], implying that alternative methods need to be developed to address the problem of P-poisoning.

Despite previous work on regenerating P-poisoned catalysts, relatively little is known about the conditions in which CePO₄ is formed. In studies regarding commercial catalysts, the effect of Paging is evaluated by comparing fresh samples and samples aged for 30,000-160,000 km in conventional automobiles [15-17]. In model systems studies the aging treatment is typically simulated by depositing phosphates by impregnation of the catalyst with NH₄H₂PO₄ solutions followed by calcination to get a final P content of 0.04-4.5 wt% [19,21,23]. In one study, CeO₂ aging was performed for only 10 h by introducing 85 ppm H₃PO₄ through the gas feed [22]. Notably, aging effects were similar in model systems and real catalysts, even if the chosen conditions, the materials studied and method of P addition were different. This suggests that model systems studies are relevant to real applications, and also that aging can be very fast as soon as phosphates reach the catalytic bed at a certain temperature of formation. Despite this, to our best knowledge, time-on-stream deactivation studies on commercial or model systems are still too limited. Also, the temperature threshold at which CePO₄ is formed was only reported by Xu et al. [22] for pure CeO₂ under lean conditions (600 °C). However, in their study, gas-phase P₂O₅ was introduced by thermal decomposition of aqueous H₃PO₄, resulting in 5% H₂O in the reaction atmosphere. In the present study, we show that the introduction of H₂O in methane combustion reaction mixture enhances the effect of phosphorus poisoning, leading to deactivation. This is particularly relevant to lean-burn engines converters and other real applications, in which water is typically present in 5–15% vol concentration [13,14].

2. Experimental method

2.1. Catalyst synthesis

Potassium tetrachloropalladate(II) (99.95%) and palladium nitrate (99.95%) were purchased from ChemPUR. Cerium ammonium nitrate (CAN, 99.99%), sodium methoxide (25% in methanol), phosphoric acid (85%), 11-mercaptoundecanoic acid (MUA, 95%), dodecanoic acid (99%), triethoxy(octyl) silane (TEOOS, 97.5%), and all the solvents (analytical grade) were obtained from Sigma–Aldrich. Sodium borohydride (98%+) was purchased from Acros Organics. Graphite foils, 0.25 mm thick, were purchased from Alfa Aesar (99.8%, phosphorus-free graphite) and ChemPUR (99%, graphite containing phosphorus). The foils were cut into 9×9 mm slides and washed with water and acetone prior to use.

The supramolecular Pd@CeO2 units were prepared according to published procedures [28]. Briefly, pre-formed Pd nanoparticles protected by 11-mercaptoundecanoic acid (MUA) were mixed with Ce(IV) tetradecyl alkoxide to obtain a Pd:Ce molar ratio of 3.70, leading to the formation of self-assembled units with an intimate Pd-Ce contact. A controlled hydrolysis in the presence of dodecanoic acid leads to the formation of the Pd@CeO2 structures, in which small crystallites (\sim 3 nm) of CeO₂ organize around the preformed metal particles. These units were deposited from solution onto the two types of graphite, one containing phosphates (P-graphite) and one pure (graphite), according to a procedure described in detail elsewhere [30]. The Pd@CeO₂ batch was diluted 1:10 and the resulting solution was added to the slide 5 times, 0.1 mL at a time, allowing the slide to dry between additions. The Pd@CeO₂/P-graphite and Pd@CeO₂-graphite model catalysts were calcined to 450 °C in air for 5 h. These samples will be referred to as "fresh".

2.2. Aging treatments

Aging treatments were performed in a U-shaped quartz reactor, using an alumina tray to hold the model-catalyst slides in place. Reactions were carried out at a total gas pressure of 1 atm, with the inlet composition controlled by varying the flow rates of CH₄, O₂ and Ar, while maintaining the total flow rate at 21.3 mL min $^{-1}$. The Gas Hourly Space Velocity (GHSV) was $10^6\,\text{mLg}^{-1}\,h^{-1}$, using the volume of Pd@CeO $_2$ dispersion added to the graphite slides.

The heating and cooling rates in all heating measurements were fixed at $10\,^{\circ}\text{C}\,\text{min}^{-1}$. For experiments that included water, the premixed, gaseous reactant mixture was bubbled through a saturator heated to the temperature required for the desired water feed concentration. The composition of the effluent gases was monitored on-line using a mass spectrometer. At the end of the aging treatment, the system was purged with Ar, cooled to room temperature, and finally stored under Ar until rapid transfer to the XPS chamber.

2.3. Characterization techniques

The X-ray Photoelectron Spectroscopy (XPS) and Synchrotron Radiation Photoelectron Spectroscopy (SRPES) experiments were carried out at the Materials Science Beamline (MSB) at the Elettra Synchrotron Light Source in Trieste, Italy. The MSB is a bending magnet beamline with a plane grating monochromator that provides light in the energy range of 21-1000 eV. The UHV endstation, with a base pressure of 1×10^{-8} Pa, is equipped with an electron energy analyzer (Specs Phoibos 150) and a dual Mg/Al X-ray source. High-resolution, SRPES measurements were performed on the following core levels (photon energies in parentheses): O 1s (610 eV), Pd 3d (610 eV), C 1s (425 eV), and P 2p (425 eV). Complementary XPS spectra of Ce 3d, O 1s, C 1s, P 2p, and Pd 3d core levels were recorded at the same end station using the excitation energy of 1486.6 eV (Al K α). The apparent degree of reduction of ceria was determined from the Ce 3d spectra using the procedure described in a previous publication [29]. Binding energies are reported after correction for charging using the graphite C 1s as a reference.

Sample surfaces were also examined by means of a field-emission Scanning Electron Microscope (SEM) (Model Tescan Mira 3). High resolution was achieved using an acceleration voltage of 30 kV and a working distance of less than 3 mm. Additionally, a Bruker XFlash® 6 | 10 Energy Dispersive Spectrometer (EDS), mounted on the SEM apparatus, was used to carry out element mapping of the sample. Characteristic X-ray radiation was excited by 20 keV primary electrons.

Atomic Force Microscopy (AFM) was performed using a Nanoscope V (Digital Instruments Metrology Group, model MMAFMLN), in tapping mode in air at room temperature, using

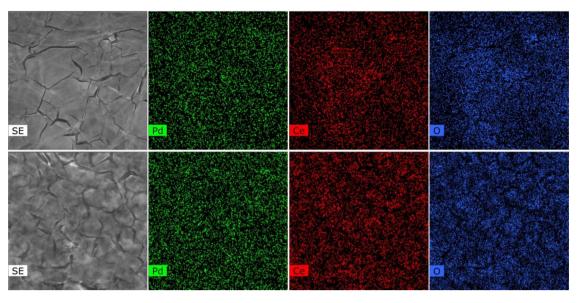


Fig. 1. 20 μm viewfield SEM images and EDS mapping of Pd, Ce and O signals of fresh Pd@CeO₂/graphite (top row) and Pd@CeO₂/P-graphite (bottom row) samples.

an n-type silicon μ mash® SPM probe (HQ:NSC15/AL BS) with tip height of 12–18 μ m and cone angle < 40° (Resonant frequency 325 kHz, force constant of \sim 40N/m).

X-ray Absorption Near Edge Structure (XANES) experiments were performed at the SAMBA beamline at Synchrotron SOLEIL (France) with a Si (220) double crystal monochromator. The monochromator was kept fully tuned and harmonics were rejected by a pair of Pd-coated, Si mirrors. Spectra were recorded in fluorescence mode at the Pd K edge ($E = 24350 \,\mathrm{eV}$) and Ce L_{III} edge $(E=5723.4\,\mathrm{eV})$ using a 35-element Ge detector. Operando experiments were conducted using the transmission and fluorescence cell described elsewhere [30]. Three slides of Pd@CeO₂/P-graphite catalyst and a total gas flow rate of 12 mL min⁻¹ (0.5% CH₄, 2.0% O₂, 15.0% H₂O if appropriate, and N₂ balance) were used for both Ce LIII edge experiments and Pd K edge experiments. Product analysis was carried out using a Cirrus-MKS mass spectrometer. The observed activity was comparable to that observed during catalytic testing. The fractions of Ce³⁺ and Pd⁰ in the samples were determined by fitting the XANES part of the spectrum using a linear combination of spectra for CePO₄ and CeO₂ to fit data for Ce and a combination of spectra for PdO and a Pd foil to fit data for Pd. All measurements were performed during the same beam session.

3. Results

The graphitic supports used in this study were analyzed by EDS to determine their P content. As expected, no P was observed on the pure graphite support, while the P-graphite samples contained 1000 ± 100 ppm of P. The P signal did not change appreciably upon deposition of Pd@CeO₂ particles, nor was it affected by any of the aging treatments performed in this study. Complementary XPS/SRPES analysis was performed on the as-received graphitic supports to determine the chemical state of phosphorus and the surface/bulk distribution. Prior to calcination, there was no P signal on either the P-graphite or the pure graphite. A phosphorus signal, at a Binding Energy (BE) corresponding to that of PO_4^{3-} (133 eV) was only observed on the P-graphite after thermal treatment to 450 °C in air (see Fig. S1). Similar treatment of the pure graphite did not cause the appearance of a P signal. This suggests that P is initially present only in the bulk of the P-graphite support and is released during the thermal treatment. An O 1s signal at 530.5 eV appeared

together with the P signal, indicating the presence of PO_4^{3-} species. This fingerprint of PO_4^{3-} was present on all $Pd@CeO_2/P$ -graphite samples, independent of aging conditions and with a similar intensity as was observed following calcination at $450\,^{\circ}$ C. In accordance with these observations, phosphates can be present as intercalating compounds of graphite foils manufactured by squeezing exfoliated graphite [31].

SEM images of the fresh Pd@CeO $_2$ /graphite and Pd@CeO $_2$ /Pgraphite catalysts are shown in Fig. 1 and exhibit very similar surfaces, displaying large, smooth domains of a continuous film, separated by small, shallow cracks. The distributions of Pd, Ce and O signals over the samples were homogeneous, demonstrating that the Pd@CeO $_2$ particles were well-dispersed and exposed to the gas phase for both supports, an important prerequisite for model catalytic systems.

The "fresh" catalysts were then aged for 0 min, 30 min, 1 h, or 9 h under catalytic reaction conditions, at 500 °C and 600 °C, in dry and wet conditions. In all experiments, the catalyst was ramped to the desired temperature in 0.5% CH₄, 2.0% O₂ and 15.0% H₂O (for wet conditions) and held at that temperature for the chosen time span. After aging, the gas flow was switched to pure Ar and the samples cooled to room temperature before being transferred to either the SRPES/XPS line or to the SEM.

As shown in Fig. 2A, the fresh model $Pd@CeO_2/graphite$ catalyst showed significant and constant evolution of CO_2 as result of CH_4 oxidation at both 500 and $600\,^{\circ}C$. While rates were stable under dry conditions, the rate of CO_2 production decreased with time at both temperatures when water was added. The $Pd@CeO_2/P$ -graphite samples were less active for methane oxidation (Fig. 2B). Most notably, there was a fast and irreversible deactivation during wet aging at $600\,^{\circ}C$. After 1 h of isothermal treatment under these conditions, the sample was almost completely inactive.

SEM images of the aged samples in Fig. 3 show differences between the catalysts supported on graphite and P-containing graphite. The surfaces of the Pd@CeO $_2$ /graphite samples were not appreciably altered by any of the aging treatments. However, images of the Pd@CeO $_2$ /P-graphite samples show features having diameters of 10–30 nm, with sizes that are slightly bigger for 600 °C aging treatments. These spots are partially sintered Pd@CeO $_2$ particles. The SEM analysis suggests that the presence of phosphorus causes partial aggregation of the Pd@CeO $_2$ units and growth of crystallite sizes that does not occur in the absence of P.

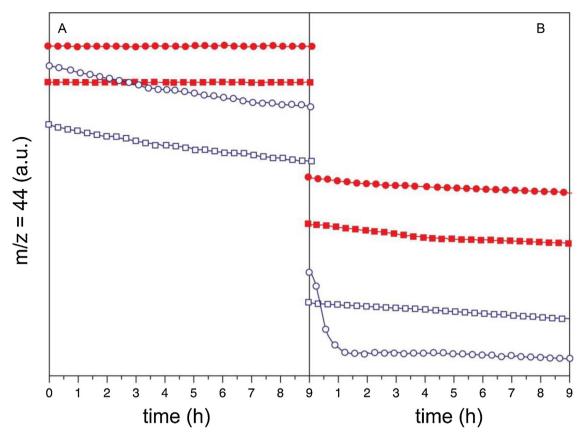


Fig. 2. CO_2 evolution over time. (A) $Pd@CeO_2/graphite$; (B) $Pd@CeO_2/P$ -graphite. Circles: 600 °C aging; squares: 500 °C aging; filled symbols: dry conditions ($CH_4 0.5\%$, $O_2 2\%$, GHSV: $10^6 mLg^{-1} h^{-1}$); open symbols: wet conditions ($15\% H_2O$ vapor added to reaction atmosphere).

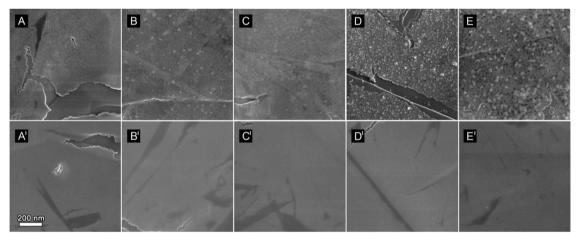


Fig. 3. SEM of Pd@CeO₂/P-graphite (A–E) and Pd@CeO₂/graphite samples (A'–E'). The samples were fresh (A, A') or treated for 9 h under the following conditions: dry reaction conditions at 500 °C (B, B') or 600 °C (D, D'); wet reaction conditions at 500 °C (C, C') and 600 °C (E, E').

Fig. 4 indicates that the Ce 3d region of the XPS spectra is very different for the Pd@CeO $_2$ /graphite and Pd@CeO $_2$ /P-graphite samples. Spectra on the Pd@CeO $_2$ /graphite samples were all similar, with features typical of pure CeO $_2$. Initially, the apparent O:Ce stoichiometry is 1.94 (12% Ce $^{3+}$) but it increases to 2.0 with aging time. Apparently, a small fraction of the cerium is in the Ce $^{3+}$ state in the initial particles but all of the Ce atoms are converted to Ce $^{4+}$ under the aging conditions used in this study. This behavior differs from that observed for Pd@CeO $_2$ /Si-Al $_2$ O $_3$ catalysts, which showed a low but constant Ce $^{3+}$ fraction for all the treatments [13]. Various factors could contribute to this, including the different surface sensitivity of the techniques used (XPS-XAS) and the different Pd:Ce

ratio, but the different calcination temperatures used here (450 °C vs 850 °C) and the different supports (Al $_2$ O $_3$ vs graphite) are likely the primary causes. On the Pd@CeO $_2$ /P-graphite sample, in contrast, the XPS spectra show mainly features of CePO $_4$ [19,32], even on the fresh sample, for which Ce $^{4+}$ is also still observed. Spectra taken after heating to 500 °C under dry and wet aging were similar to each other and showed only small changes compared to the fresh sample. On the other hand, aging treatments at 600 °C resulted in dramatic changes. After 30 min of wet aging at this temperature, the Ce $^{4+}$ signal completely disappeared. Spectra obtained after prolonged dry aging (9 h) showed partial oxidation to Ce $^{4+}$ with respect to the fresh sample.

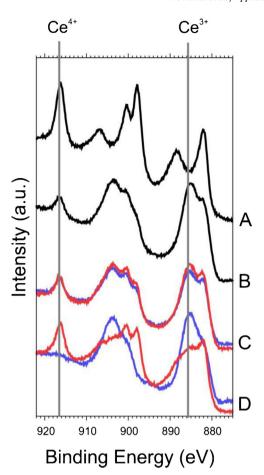


Fig. 4. Representative Ce 3d XPS spectra of: (A) the fresh Pd@CeO₂/graphite sample; (B) fresh Pd@CeO₂/P-graphite; (C) Pd@CeO₂/P-graphite aged at $500\,^{\circ}$ C; (D) Pd@CeO₂/P-graphite aged at $600\,^{\circ}$ C. Dry conditions are shown by red lines and wet conditions by the blue lines. The areas of the presented spectra have been normalized after subtraction of Shirley background and the curves have been offset for clarity. The positions of the most prominent peaks in Ce⁴⁺ and Ce³⁺ spectra are marked by grey lines. (For interpretation of the references to color in this figure legend, the reader is referred to the web version of this article.)

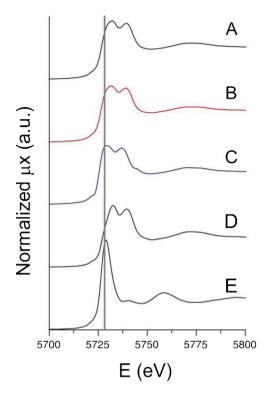


Fig. 6. Operando XANES spectra of $Pd@CeO_2/P$ -graphite sample at $Ce\ L_{III}$ edge: (A) fresh; (B) during dry aging at $600\,^{\circ}C$; (C) during wet aging at $600\,^{\circ}C$. Reference spectra: CeO_2 (D), $CePO_4$ (E).

Fig. 5 shows the percentage of Ce³⁺ on the Pd@CeO₂/P-graphite sample for the different aging conditions. Since, in the absence of P, the Ce in the Pd@CeO₂ particles is almost completely oxidized to Ce⁴⁺ after the initial calcination and after all aging treatments, the trends observed for the Ce³⁺ percentage in this case are indicative of CePO₄ formation on the surface of the particles sampled by XPS. The fresh sample contains 75% Ce³⁺, demonstrating that the particles are extensively covered by CePO₄ already after calcination. For aging at 500 °C, the percentage of Ce³⁺ does not change appreciably, regardless of the aging conditions (dry or wet). However, aging at 600 °C changed the sample dramatically. Wet aging caused an increase in Ce³⁺ percentage to 100% after 30 min, while dry aging decreased the Ce³⁺ content, to 40% Ce³⁺ after

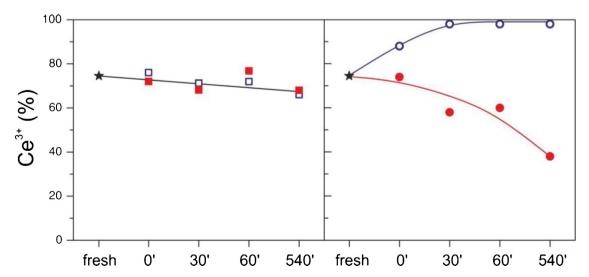


Fig. 5. Calculated Ce3⁺ percentage for Pd@CeO₂/P-graphite samples, determined by fitting of Ce 3d XPS spectra. Fresh samples: star. Squares: aged at 500 °C (filled: dry conditions, empty: wet conditions). Circles: aged at 600 °C (filled: dry conditions, empty: wet conditions). The solid lines are guides to the eye.

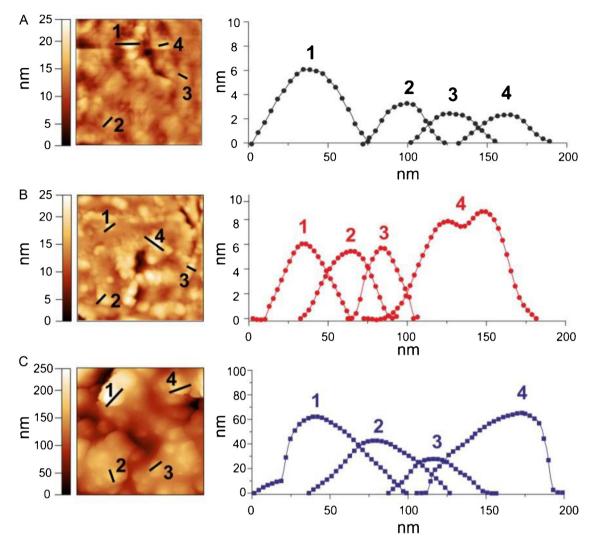


Fig. 7. AFM topography images with representative line scans for Pd@CeO₂/P-graphite: (A) fresh; (B) aged at 600 °C under dry conditions for 9 h; (C) aged under wet conditions at 600 °C for 9 h. Please note the different scales in part C.

9h. These results indicate a crucial role for water in the formation, accumulation, and stabilization of phosphates on ceria.

To gain further insights into the extent of CePO₄ formation and the extent of cerium reduction, *operando* and *ex-situ* XANES measurements were performed on the Pd@CeO₂/P-graphite catalysts, with representative results shown in Fig. 6. In all cases, only minor differences were observed between fresh, dry-aged and wet-aged samples, at both 500 °C and 600 °C. In contrast to the XPS results, the Ce³⁺ percentage did not evolve during aging treatments and ranged from 15% to 18% in all the samples studied. Indeed, these results are similar to recent *in-situ* EXAFS data on a Pd@CeO₂/Si-Al₂O₃ powder having a similar Pd@CeO₂ composition with no P poisoning. That study also indicated the presence of 20% Ce³⁺ in the fresh catalyst [13].

The dramatic difference in the valence ratios calculated from XPS and XANES implies that the surface and bulk concentrations can be very different on these samples. Since the inelastic mean free path in CeO₂ of the photoelectrons originating from Ce 3d level in the XPS study is approximately 1.2 nm and the expected dimensions of the CeO₂ crystallites in the Pd@CeO₂ particles is 3–4 nm [6,30], the large difference between surface and bulk concentrations cannot be explained by the presence of CePO₄ at the surface of the initial Pd@CeO₂ core–shell particles. Rather, the data indicate that thermal sintering or partial aggregation of ceria crystallites must occur under wet aging at 600 °C.

To further investigate the evolution of the Pd@CeO₂ particles dimensions during aging, the Pd@CeO2/graphite and Pd@CeO2/Pgraphite samples were characterized by AFM topographic analysis. Fig. 7 shows images and height profiles for the Pd@CeO₂/P-graphite sample, both fresh and after 9-h aging at 600°C. Results for the Pd@CeO2/graphite sample are not shown but were essentially identical to that observed for fresh Pd@CeO2/P-graphite, even with various aging treatments. For both Pd@CeO2/graphite and Pd@CeO2/P-graphite, the fresh and dry aged samples showed small features, approximately 10 nm in height, similar to what was observed for Pd@CeO2 particles deposited onto YSZ(100) single crystals [33] (Fig. 7A and B). Wet aging did not appreciably change the Pd@CeO₂/graphite sample at either 500 °C or 600 °C. However, wet aging at 600 °C caused dramatic sintering on the Pd@CeO₂/P-graphite sample, leading to the appearance of features that were 50-60 nm high and 50-70 nm wide, distributed over a corrugated surface (Fig. 7C). The changes in particle size help explain how the bulk and surface compositions can be so different.

Fig. 8 shows XPS/SRPES spectra for the O 1s region of the Pd@CeO₂/graphite and Pd@CeO₂/P-graphite samples and the results support the conclusions reached from the Ce 3d core level. The spectrum of the fresh Pd@CeO₂/graphite sample, Fig. 8A, shows two peaks at 529.2 eV and 531.6 eV. The peak at lower BE can be assigned to bulk CeO₂, while the higher BE peak is likely due to hydroxyl species [34]. However, the presence of

other species having similar BE cannot be entirely ruled out. Carbonates arising from reaction with the graphite supports are not expected to form during the thermal treatments performed here; also, similar O 1s spectra were observed for Pd@CeO2 on Au (not reported here). When the Pd@CeO₂/graphite sample was aged under wet conditions, Fig. S2, the intensity of the peak at 532 eV was enhanced and a slight shift to higher binding energies was observed, further supporting the assignment of the signal to hydroxyl species [9,13,34]. With Pd@CeO₂/P-graphite, the spectrum of the fresh sample, Fig. 8B, again showed a peak near 529 eV due to bulk CeO₂ but the largest peak was centered at 530.4 eV, which can be assigned to CePO₄ based on the preliminary analysis performed on the P-containing graphite. There was very little change in the spectrum of samples aged under dry conditions at either 500 °C or 600 °C, but wet aging at either temperature gave increased intensity in the region assigned to hydroxyls. After wet aging at 600 °C, the peak associated with bulk CeO₂ essentially disappeared. This is consistent with the disappearance of the Ce⁴⁺ signal in the Ce 3d region of the 600 °C wet-aged samples.

XPS spectra of the Pd 3d region on representative samples are shown in Fig. 9. For both Pd@CeO $_2$ /graphite and Pd@CeO $_2$ /Pgraphite, the fresh samples show two peaks at 337.2 eV and 342.4 eV, which are almost certainly due to PdO. The two peaks are due to the Pd spin–orbit split doublet (Pd 3d $_{5/2}$ and Pd 3d $_{3/2}$). The BE of the doublet is actually close to the BE expected for PdO $_2$ [35]; however, a shift to higher binding energy is often observed for metal and metal–oxide nanoparticles, including Pd and PdO [36–42]. For example, the 3d $_{5/2}$ signals of both PdO and Pd nanoparticles have previously been reported to shift to approximately 1.0 eV higher BE due final-state effects [36,40]. The fact that our samples contained PdO was confirmed by *operando* and *ex-situ* XANES measurements on both the graphite and P-graphite supported catalysts (Fig. S4).

Neither wet nor dry aging had any effect on the XPS spectrum for Pd on the Pd@CeO₂/graphite sample; however, the same was not true for Pd@CeO₂/P-graphite. While dry aging did not affect the spectrum, wet aging of the P-containing sample at 600 °C resulted in the complete disappearance of the Pd signal. Since EDS and XANES results demonstrate that Pd is not lost under these conditions (Fig. S4), the loss of Pd signal in XPS must be due to burial of Pd under the CePO₄. This agrees with the SEM results, showing that the Pd@CeO₂ particles undergo severe sintering during wet aging when P is present.

4. Discussion

One of the main objectives of this work was to study the effect of P-poisoning on the catalytic performance of Pd-CeO₂ catalysts. Similarly to other P-poisoning studies, phosphorus was deliberately introduced in the system during the catalyst preparation [19,21,23], rather than introducing it from the gas feed during aging treatments [22]. In this way, H_2O is not introduced in the reaction mixture by decomposition of H₃PO₄ to P₂O₅ and the effect of water addition can be studied separately. The combined results in this study demonstrate that the presence of phosphorus in the vicinity of a Pd/ceria catalyst results in the rapid formation of CePO₄ at temperature as low as 450 °C. Since vapor pressure of phosphates is negligible under these conditions, the formation of CePO₄ indicates that there is a high affinity of Ce and P. This agrees with previous results from Xu et al., who observed formation of CePO₄ from the reaction of CeO₂ with AlPO₄ [22]. Notably, the distribution of CePO₄ in the surface and subsurface of CeO₂ particles is in agreement with other observations from the literature [19,22–25], even if the source of phosphorus and aging conditions were different.

Interestingly, the phosphorous-poisoned catalysts maintain a relatively high activity under dry conditions, despite being

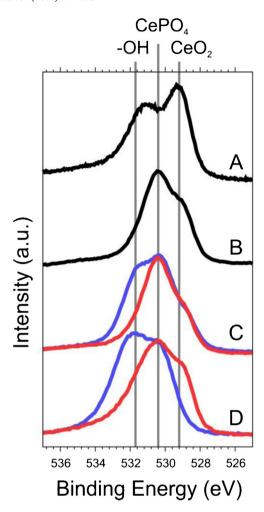
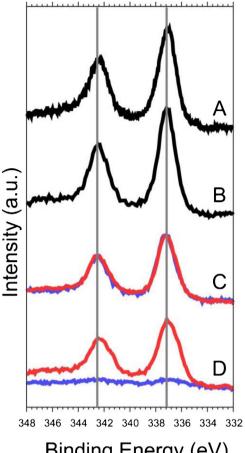


Fig. 8. Representative O 1s XPS spectra: (A) fresh Pd@CeO₂/graphite; (B) fresh Pd@CeO₂/P-graphite; (C) Pd@CeO₂/P-graphite aged at $500\,^{\circ}$ C; (D) Pd@CeO₂/P-graphite aged at $600\,^{\circ}$ C. The red lines were obtained after aging under dry conditions and the blue lines under wet conditions. The areas of the presented spectra have been normalized to the CePO₄ contribution (B–D) and the P free sample (A) has been adjusted to comparable intensity. The curves have been offset for clarity. The positions of assigned O 1s contributions are marked with grey lines. (For interpretation of the references to color in this figure legend, the reader is referred to the web version of this article.)

extensively covered by phosphates. Indeed, the XPS spectra even indicate that cerium phosphate can be partially removed from the surface of ceria particles at $600\,^{\circ}$ C under dry conditions. In agreement with this, López Granados et al. reported that, on P-poisoning of CeO₂ by addition of $(NH_4)_2HPO_4$, followed by calcination to $600\,^{\circ}$ C [19] some of the CeO₂ surface was not converted to CePO₄ and was still available for oxygen exchange with gas-phase oxygen, even for samples having a high P:Ce ratio.

The presence of water changes things completely, and a rapid, irreversible deactivation is observed at temperatures above 600 °C. At these temperatures, CePO₄ becomes highly mobile and causes severe aggregation of ceria particles and Pd encapsulation. The results of this study indicate that water and phosphorus have a cooperative effect and take part in a deactivation mechanism activated by high temperature. For the first time, the deactivation of Pd-CeO₂ catalysts in the presence of P was studied in steady-state experiments, revealing that poisoning occurs in very short time under conditions relevant for real applications [22,23,25]. Although surface blockage by CePO₄ is reported in the literature as the main effect of P-poisoning on ceria-based catalysts, our work reveals that phosphorus can



Binding Energy (eV)

Fig. 9. Representative Pd 3d XPS spectra: (A) Pd@CeO₂/graphite; (B) fresh Pd@CeO₂/P-graphite; (C) Pd@CeO₂/P-graphite aged at 500°C; (D) Pd@CeO₂/P-graphite aged at 600°C. Aging under dry conditions is indicated by the red lines while wet aging is indicated in blue. The curves have been offset for clarity. (For interpretation of the references to color in this figure legend, the reader is referred to the web version of this article.)

also cause deep morphological transformations of the catalyst and dramatic loss of activity, especially in the presence of water.

5. Conclusions

The effect of phosphorus poisoning on the catalytic combustion of methane over $Pd@CeO_2/graphite$ catalysts was found to be dramatically influenced by temperature and presence of H_2O . When P was not introduced in the catalyst formulation, the catalysts were active and stable under all studied conditions (500–600 $^{\circ}\text{C}$; dry and wet conditions). On the other hand, P-poisoned catalysts were less active and stable because of partial thermal sintering. Water vapor causes rapid and complete deactivation at higher temperatures by inducing severe aggregation of ceria nanoparticles, incorporation of Pd active phase in the bulk of the crystallites and exposure of CePO_4 to the catalyst surface. The combination of XPS/SRPES, operando XANES measurements, SEM/EDS and AFM techniques provides evidence of a temperature dependent, water-driven P-poisoning of Pd and CeO_2-based oxidation catalysts.

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Appendix A. Supplementary data

Supplementary data associated with this article can be found, in the online version, at http://dx.doi.org/10.1016/j.apcatb.2015.10.001.

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